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# Simulating of synergistic phenomena ionic solutions encountered in extraction uranium process

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# Context

### **Current AMEX process, a liquid-liquid extraction**

**The leachate** is an aqueous solution obtained after the mining process. It contains uranium sulfate, sulfuric acid and impurities. It is further contacted with an **organic phase** containing an extractant,  $(TOAH^+)_2SO_4^{2-}$ , a linear alkane and a phase modifier: 1-octanol.

After **demixtion**, uranyl is transferred in the organic phase thanks to the formation of aggregates with the extractant.

Formation of third hase without phase modifier

**Problems** of this process are the selectivity toward the others species, the need of a phase modifier to avoid 3<sup>rd</sup> phase formation, and the loss of the diluent due to evaporation.

### New process proposed by LTSM (1)

Contacting the leachate with an **ionic liquid** of  $(TOAH^+)_2SO_4^{2-}$ , without diluent and phase modifier.

With this new process, loading capacity of uranyl in the ionic phase is significantly increased. We obtain better separation factors towards the impurities like vanadium, iron, zirconium, molybdenum ... and due to the absence of linear alkane, the solvent loss is close to zero.

 $(TOAH^+)NTf_2^-$  is added as it presents a smaller viscosity. The mixture  $(TOAH^+)_2SO_4^{2-}$ +  $(TOAH^+)NTf_2^-$ should give a linear response : it should decrease linearly the loading charge of uranyl and the viscosity, but it doesn't.

However, the **viscosity is 200 times higher** than the one of the current AMEX process, which is a problem for industrial application.





We model atoms and ions like beads 1 Å with force fields

10 Å

 $10^2$  Å



 viscosity after conctact viscosity before conctact Formation of aggregates spontaneously





# **Methods**

We used **non polarizable classical molecular dynamics** with AMBER 20 and PMEMD package (3).

We used a 12-6-4 Lennard jones potential.

 $V(r_{ij}) = 4\epsilon_{ij} \left( \left(\frac{\sigma_{ij}}{r_{ij}}\right)^{12} - \left(\frac{\sigma_{ij}}{r_{ij}}\right)^6 \right) + \frac{e^2 q_i q_j}{r_{ij}} - \frac{C_4^{ij}}{r_{ij}^4}$ 

**Equilibration** of the box in the **NPT ensemble**, the number of atoms (N), the pressure (P) and the temperature (T) are constant. We need a equilibration phase in this thermodynamic ensemble to have the correct density, energy and structure of the system.

**Production** runs in the **NVT ensemble**, at constant volume (V), in order to launch the simulations on graphical processing units GPUs which is 20 times faster.



OPC 4 points model for<br/>water molecule (4)Protanated<br/>trioctylamine



## Small Angle X-ray Scattering (SAXS) by MD simulation (2)

Uranium charge capacity

 $-\blacksquare [TOAH]_2[SO_4] + [TOAH][NT]$ 

The SAXS intensity is calculated from MD simulation

$$I(q) = \sum_{\alpha} \sum_{\beta} f_{\alpha}(q) f_{\beta}(q) \sqrt{N_{\alpha} N_{\beta}} S_{\alpha\beta}$$

With  $S_{\alpha\beta}$  the structure factor between the species  $\alpha$  and  $\beta$ 

$$S_{\alpha\beta} = \delta_{\alpha\beta} + 4\pi \sqrt{\rho_{\alpha}\rho_{\beta}} \int_0^r (g(r) - 1) \frac{\sin(qr)}{qr} r^2 dr$$

 $f_{\alpha}(q)$  is the form factor of the species  $\alpha$  $N_{\alpha}$  is the number of atom  $\alpha$  $\rho_{\alpha}$  is the density of atom  $\alpha$ g(r) the radial distribution function  $\delta_{\alpha\beta}$  is the kronecker delta

Theoretical intensity are compared with experiment
 Interpreting the experimental results by identifying which

contribution gives a peak

# **Densities**

# SAXS

**Densities for different concentrations** of  $(TOAU^+)$   $SO^{2-}$  and  $(TOAU^+)$   $NTf^-$ 

Comparison of the experimental and theoretical SAXS intensity without uranyl
> attribution the origins of each peak



- □ No simulation yet at low concentration of uranyl due to the need of a big simulation box for the ratio between 0 and 50% of  $(TOAH^+)_2SO_4^{2-}$ .
- □ Same trend: the density decreases for high percentage of  $(TOAH^+)_2SO_4^{2-}$ .
- □ Small differences between simulations and experiments. There are several possible explanation:
  - An experimental systematic error due to the measure
  - Different composition because of impurities and water
  - The force fields for the different molecules are not good
  - The protonation states of species as a function of the percentage of  $(TOAH^+)_2SO_4^{2-}$ .



# Box with low concentration of uranyl

#### We need a big box to simulate low concentrations

Because the  $(TOAH^+)NTf_2^-$  doesn't extract, the ratio with 0% of  $(TOAH^+)_2SO_4^{2-}$  has a very low concentration of uranyl :  $5.80 \times 10^{-6}$  mol/L. To simulate this concentration, we need a cubic box of 550 Å with 50 000 TOAH : It's too much!

For now, we tried to simulate a cubic box of 200 Å with 10 000 TOAH, but we have no uranyl in the box at the lowest concentration. We glue 8 small boxes together to fasten the calculations.



# **Outlook and conclusions**

- We made a lot of simulation with and without uranyl to compare the MD results with experiments
- □ We obtained the same trend for the density with a small difference with experiment
- We calculated the same SAXS intensities with 3 peaks at the same positions allowing to explain the structure of the solution
- □ The next step will be to compare theoretical and experimental EXAFS spectra in order to look at the first coordination shell of the uranyl complexes.

□ All these results **confirm the 12-6-4 force field** of the uranyl

## References

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