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1 **Raw dark fermentation effluent to support heterotrophic microalgae**
2 **growth: microalgae successfully outcompete bacteria for acetate**

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9 **Abstract**

10 Coupling dark fermentation (DF), which produces hydrogen from diverse effluents or solid
11 waste, and heterotrophic cultivation of microalgae, which produces lipids, carbohydrates and
12 proteins, is a promising and innovative solution for developing sustainable biorefineries. The
13 use of a raw DF effluent, containing acetate and butyrate, to support the heterotrophic growth
14 of *Chlorella sorokiniana* was investigated. All the acetate in sterilized and unsterilized DF
15 effluent was exhausted in less than three days of heterotrophic cultivation, whereas butyrate
16 was not used by the microalgae. The microalgae biomass reached 0.33 g L⁻¹ with a carbon
17 yield on acetate of 55%. The algal yield was higher than previously reported for synthetic DF
18 effluent. It was concluded that compounds other than volatile fatty acids were present in the
19 DF effluent and these could be consumed by the microalgae. After the acetate had been
20 exhausted, butyrate was consumed by facultative and strict aerobic bacteria originating from
21 the DF effluent. The concentration of the bacterial community increased during the
22 experiment but did not have any significant impact on heterotrophic microalgae growth. A
23 high microalgal biomass yield was achieved without requiring the DF effluent to be sterilized.

1 **Keywords**

2 Biohydrogen, Heterotrophic cultivation, Dark fermentation, Volatile Fatty Acids (VFAs),
3 Bacterial diversity, *Chlorella sorokiniana*

4 **1 Introduction**

5 Over the past decade, increasing attention has been paid to the growth of microalgae in
6 heterotrophic conditions, i.e. in the dark using organic carbon sources, due to (i) high growth
7 rates, biomass densities and lipid yields achieved, (ii) the possibility of using non-arable land,
8 (iii) high volumetric production and (iv) the use of existing technologies, such as microbial
9 fermenters [1]. Heterotrophic microalgae can be cultivated to produce either low-added value
10 molecules such as lipids for biofuels, or high-added value molecules such as the omega 3 fatty
11 acids, DHA and EPA, for human nutrition [2]. However, owing to the high cost of the most
12 common substrate, glucose, using heterotrophic microalgae is only currently economically
13 competitive for human nutrition [3].

14 In recent years, coupling bacterial dark fermentation (DF), to produce hydrogen, and
15 heterotrophic cultivation of microalgae, to produce lipids, has been suggested as being a very
16 promising sustainable approach for producing gaseous and liquid biofuels [4]. DF is a simple
17 process that can convert a wide range of solid waste and effluents into hydrogen, a high-
18 energy gas [5]. During DF, anaerobic bacteria break down complex carbon compounds from
19 the organic matter contained in waste (e.g., food waste or agricultural waste) and wastewater
20 (e.g., wastewater from agriculture, the paper industry or the sugar industry) into simple
21 organic acids [6]. Acetic and butyric acids are the two main end products of DF and can be
22 further used as low cost carbon sources to sustain the growth of heterotrophic microalgae [7].
23 The main advantage of DF is that organic carbon compounds from complex waste that are not
24 directly available to microalgae degradation are simplified into low molecular weight volatile

1 fatty acids (VFAs) [8]. DF effluents also contain substantial amounts of nitrogen and
2 phosphorus that are required to sustain the heterotrophic growth of microalgae. Cho *et al*
3 pointed out that DF effluent can be regarded as a good medium for growing heterotrophic
4 microalgae in a biorefinery [9].

5 Recent studies investigating microalgae growth on a synthetic DF effluent medium showed
6 very promising results. When grown heterotrophically on a mixture of acetate and butyrate,
7 *Chlorella protothecoides* reached a carbon yield, (g carbon of biomass per g carbon of VFAs)
8 of 34% and a lipid content of 48% of cellular dry weight (CDW) [3]. Turon *et al.* [10]
9 reported that *Chlorella sorokiniana* could grow heterotrophically on acetate with a growth
10 rate of 2.23 d⁻¹ and a carbon yield of 42% and on butyrate with a much lower growth rate of
11 0.16 d⁻¹ and a carbon yield of 56%. Recent studies showed that heterotrophic microalgae
12 growth was possible using sterilized DF effluents. For example, heterotrophic *Scenedesmus*
13 *sp.* produced lipids up to 41% of CDW using acetate from sterilized DF effluent containing
14 ethanol but no butyrate [7]. *Chlorella vulgaris* was grown in heterotrophic conditions on
15 diluted DF effluent containing acetate and butyrate, converting VFAs efficiently into
16 carbohydrates (51% CDW) [11]. Furthermore, *Chlorella sp.* was recently reported to produce
17 lipids up to 26% of CDW under mixotrophic conditions with raw DF effluent as a medium
18 [12]. For both raw and synthetic effluents, butyrate concentration has been identified as a key
19 factor driving the effective coupling of DF and heterotrophic cultivation of microalgae under
20 heterotrophic or mixotrophic conditions. Although acetate can be efficiently converted into
21 lipids, butyrate uptake by microalgae is much slower and can reduce the microalgae growth
22 when both VFAs are present. This problem can be solved either by increasing the initial
23 microalgae biomass or by increasing the initial acetate:butyrate ratio [11,13].

24 To couple DF and heterotrophic cultivation of microalgae efficiently, the cost of effluent
25 sterilization has to be reduced. According to Park *et al*, sterilization of the medium accounts

1 for more than a quarter of the investment cost of the process when coupling DF and
2 oleaginous yeast cultivation [4]. The importance of being able to use an unsterilized medium
3 to support microalgae growth was also emphasized by Ramos Tercero *et al.* [14]. Bacterial
4 contamination is one of the main challenges to be faced for upscaling heterotrophic
5 cultivation [15]. During heterotrophic cultivation, the competition between microalgae and
6 bacteria is usually found to be unfavorable to microalgae, limiting the availability of carbon,
7 nitrogen, phosphate and oxygen [16,17]. Nevertheless, these authors suggested that some
8 conditions may be favorable to microalgae growth, such as a low initial bacterial density and
9 high initial nutrient loads.

10 This work set out to determine, for the first time, the role and importance of the bacterial
11 community present in raw DF effluent on microalgae growth for coupling DF and microalgal
12 heterotrophic cultivation. *Chlorella sorokiniana* was used as a model for heterotrophic
13 microalgae because of its high growth rate on acetate and its ability to produce high amounts
14 of lipids up to 61.5% of its CDW [10,18]. The dynamics of biomass growth and carbon yield
15 of *C. sorokiniana* were evaluated using sterilized and unsterilized, raw DF effluent and the
16 biomass and diversity of bacterial community originating from the DF effluent were evaluated
17 for the unsterilized DF effluent.

18 **2 Materials and methods**

19 **2.1 Dark fermentation test batches**

20 Five identical test batches of “DF effluent” were produced simultaneously in 600 mL glass
21 bottles with a working volume of 200 mL. No culture medium was added or removed during
22 the fermentation. The culture medium consisted of 100 mM of 2-(*N*-morpholino)
23 ethanesulfonic acid (MES) buffer, 5 g L⁻¹ of glucose and 5 mL L⁻¹ of a micronutrient solution.
24 The composition of the micronutrient solution is fully described by Pierra *et al.* [19]. The

1 medium was supplemented with 1 mL L⁻¹ of F/2 medium vitamin solution (CCAP,
2 <http://www.ccap.ac.uk/>). The flasks were inoculated with 1 mL of heat-treated (15 min at
3 90 °C) anaerobic sludge from an anaerobic digester treating waste from a sugar processing
4 plant (Marseille, France). The initial substrate to biomass ratio S:X was 40, S representing the
5 initial chemical oxygen demand (COD) of the substrate (in gCOD L⁻¹) and X representing the
6 initial inoculum (in g of total volatile solids L⁻¹). To ensure anaerobic conditions, the flasks
7 were sealed and flushed with nitrogen gas as described elsewhere [19]. The pH was adjusted
8 to 6 and the bottles were incubated at 37 °C until the glucose was completely exhausted. At
9 the end of the growth phase, i.e. glucose exhaustion and hydrogen accumulation, the five
10 anaerobic cultures batches were mixed to produce the “DF effluent”. The pH of the DF
11 effluent was increased to 6.5 with 1 M NaOH. VFAs, and the ammonium and phosphate
12 concentrations were measured. Half of the DF effluent was centrifuged three times at 15,000
13 rpm for 15 min. A fraction of the supernatant was sterilized using Acrodisc® PF syringe filter
14 with 0.8/0.2 µm pores (PALL). The sterilized and unsterilized DF effluent samples were then
15 stored at 4 °C until the start of the experiment.

16 **2.2 Axenic microalgae strain and preparation of the microalgae stock culture**

17 *Chlorella sorokiniana* (CCAP 211/8K) was cultivated axenically in 500 mL Erlenmeyer
18 flasks with a working volume of 200 mL. A modified BG11 medium was used as described
19 by Turon *et al.* [10]. Sodium bicarbonate (10 mM), ammonium chloride (5 mM) and
20 dipotassium phosphate (0.31 mM) were used as inorganic carbon (C), nitrogen (N) and
21 phosphorus (P) sources, respectively. All the components of the medium as well as the flasks
22 were sterilized by autoclaving at 121 °C for 20 min before use. The flasks were incubated
23 under autotrophic conditions (light intensity of 100 µmol photons m⁻² s⁻¹) at 25 °C for 7 days.

2.3 Heterotrophic microalgae growth on dark fermentation effluent

A fixed volume of either the sterilized or the unsterilized DF effluent (36 mL) was placed in sterile 125 mL black Erlenmeyer flasks sealed with a cotton wool plug. Four mL of microalgae culture, 0.2 g L^{-1} , were added to each flask. The flasks were then incubated on a rotary shaker (150 rpm) at $25 \text{ }^\circ\text{C}$ for 10 days in complete darkness. A 1 mL sample of the culture was taken every day to measure the optical density (OD), VFA concentration, microbial concentration and diversity. The experiment was carried out in triplicate. During the whole of the experiment, the microalgae cultures in the sterilized DF effluent were checked for other living organisms every day by DAPI counterstaining and contrast phase microscopy.

2.4 Microbial analysis

2.4.1 Microalgae biomass measurement

The microalgae growth was quantified on sterilized DF effluent by measuring the OD at 800 nm (OD_{800}) as described by Turon *et al* [10]. The relationship between the cellular dry weight (CDW) and OD_{800} was determined for a wide range of CDW ($0 - 1.4 \text{ g L}^{-1}$) by filtering 15 mL of algal samples onto pre-weighed GF/F Whatman® filters that were then dried overnight at $105 \text{ }^\circ\text{C}$, giving the following calibration function.

$$\text{CDW (g L}^{-1}\text{)} = 1.24 * \text{OD}_{800} \text{ (R}^2 = 0.95\text{)}.$$

For calculating the biomass yield, the carbon content was estimated at 50% of microalgae biomass [20].

Because of the presence of small suspended solids in the unsterilized DF effluent, optical density measurement was not used for monitoring the algal biomass. As the chlorophyll content of microalgae during heterotrophic cultivation can change, this is not suitable for monitoring the microalgae growth accurately [21]. Therefore, the dynamics of microalgae

1 biomass growth were monitored by amplification of 18S rDNA gene copies, in cultures
2 carried out using both sterilized and unsterilized DF effluent.

3 **2.4.2 DNA extraction and purification**

4 700 µL of the culture sample was centrifuged at 10,000 rpm for 10 min and genomic DNA
5 was extracted using the PROMEGA Wizard® Genomic DNA Kit and then purified using the
6 QIAamp DNA Mini Kit (Qiagen).

7 **2.4.3 Quantitative PCR for microalgae (18S rDNA gene)**

8 The microalgae biomass was quantified using quantitative PCR (qPCR) and specific primers
9 for *Chlorophyta* 18S rDNA INT-4F (5' TGGTGAAGTGTTCGGATTGG 3') and INT-5R (5'
10 ARGTTG GGAGG GTTTA ATGAA 3') as described by Hoshina *et al* [22]. The quantitative
11 amplification reaction was carried out with 5 µL of DNA sample, 12.5 µL of Universal
12 SYBR® Green Supermix (Biorad) (composed of polymerase, dNTPs and SYBR® Green
13 dye), 1 µL of forward primer INT-4F, 1 µL of reverse primer INT-5R and 5.5 µL of H₂O, for
14 a total volume of 25 µL. The PCR was run in a 100 Touch™ thermal cycler equipped with a
15 CFX96™ Real-Time System (Bio-rad). There was an initial incubation of 3 min at 95 °C
16 followed by 40 cycles of denaturation-amplification (10 s at 95 °C and 30 s at 56 °C). Data
17 analysis was carried out with the Bio-rad CFX Manager software, version 3.0. A linear
18 standard curve was obtained from each assay by amplification of eight 10-fold dilutions of a
19 reference plasmid to count the number of 18S rDNA copies accurately. The reference plasmid
20 (pEX-A2 plasmid, Eurofins MWG Operon) was created using the *Chlorella sorokiniana* 18S
21 rDNA sequence published in the European nucleotide archive under the sequence number
22 X62441.2 (ENA, <http://www.ebi.ac.uk/ena>). The PCR product from the reference plasmid and
23 *Chlorella sorokiniana* DNA extracts corresponded to a 77 bp sequence (from 1666 to 1742
24 NT):

25 **TGGTGAAGTGTTCGGATTGGCGACCGGGGGCGGTCTCCGCTCTCGGCCGCCGA**

1 GAAGTTCATTAACCCTCCCACCT (the bold letters correspond to the qPCR primer
2 targets). The cycle threshold (CT), i.e. the number of cycles at which the reaction became
3 exponential, was used to quantify the number of gene copies. A linear standard curve was
4 obtained by plotting the CTs of the dilutions of the reference plasmid against the logarithms
5 of the known number of gene copies of the different dilutions of the reference plasmid. The
6 CT of each sample was then compared to the linear standard curve and the number of gene
7 copies per sample was determined. The total number of 18S rDNA gene copies per sample
8 was finally expressed as the logarithm of the number of target copies per mL of culture
9 sample. For SYBR® Green assays, the specificity of the PCR products was checked by a
10 melting curve analysis using the dissociation protocol from the Bio-rad CFX Manager
11 software. An initial incubation of 3 min at 95 °C and 40 cycles of denaturation (10 s at 95 °C
12 and 30 s at 56 °C) were performed.

13 **2.4.4** *Quantitative PCR for bacteria (16S rDNA)*

14 For quantification of total bacteria, general bacterial primers, BAC338F and BAC805R, and
15 the associated probe, BAC16F, were used as described elsewhere [23]. The quantitative
16 amplification reaction was carried out in a total volume of 12.5 µL with 2 µL of sample DNA,
17 6.5 µL of Universal probes Supermix (Biorad), 0.5 µL of each primers and the probe and 2.5
18 µL of H₂O. The thermal cycler and analysis method were the same as for qPCR of
19 *Chlorophyta*. An initial incubation of 2 min at 95 °C followed by 40 cycles of denaturation-
20 amplification (7 s at 95 °C and 25 s at 56 °C) were performed. The linear standard curve was
21 obtained as described elsewhere [24]. The total number of 16S rDNA gene copies per sample
22 was expressed as the logarithmic value of the number of target copies per mL of culture
23 sample.

1 **2.4.5 *Sequencing of bacterial 16S rDNA***

2 Samples taken on day 0, at day 2.7 and on day 10 (9 samples in total) were used for
3 sequencing. The V4-V5 region of the 16S rDNA gene was amplified over 30 amplification
4 cycles at an annealing temperature of 65 °C, with the forward primer
5 5'-CTTTCCCTACACGACGCTCTTCCGATCTGTGYCAGCMGCCGCGGTA-3' and the
6 reverse primer
7 5'-GGAGTTCAGACGTGTGCTCTTCCGATCTCCCCGYCAATTCMTTTRAGT-3' with
8 their respective linkers. In a second PCR reaction of 12 cycles, an index sequence was added
9 using the primers
10 AATGATACGGCGACCACCGAGATCTACACTCTTTCCCTACACGAC and
11 CAAGCAGAAGACGGCATACGAGAT-index-GTGACTGGAGTTCAGACGTGT. The
12 resulting PCR products were purified and loaded onto the Illumina MiSeq cartridge according
13 to the manufacturer's instructions for sequencing 250 bp reads. Sequencing was carried out at
14 the GeT PlaGe sequencing center of the Genotoul life science network in Toulouse, France
15 (get.genotoul.fr). 595799 forward and reverse sequences were retained after assembly and
16 quality checking using a slightly modified version of the standard operation procedure
17 described by Kozich *et al.* [25]. Mothur version 1.33.0. SILVA release 102 provided by
18 Schloss *et al.* [26] was used for alignment and as a taxonomic outline. A 2% dissimilarity
19 threshold was used to define OTUs in Mothur. The known species that were phylogenetically
20 closest to OTUs with a relative abundance of more than 2% at the start of the experiment (day
21 0), at acetate exhaustion (day 2.7) or at the end of the experiment (day 10) were identified
22 using the Basic Local Alignment Search Tool (BLAST) [27]. The sequences identified as *C.*
23 *sorokiniana* chloroplast were removed before analysis of bacterial abundance.

1 **2.5 Chemical analysis**

2 Acetate, propionate, butyrate, iso-butyrate, valerate, iso-valerate and caproate were measured
3 using a gas chromatograph (GC 3900 Varian) equipped with a flame ionization detector.

4 Other non-volatile molecules such as glucose, ethanol, lactate and formate were quantified
5 using HPLC with a refractive index detector and an Aminex HPX-87H column (Biorad®).

6 The column temperature was maintained at 35 °C and the flow rate at 0.4 mL min⁻¹ [28].

7 Biogas production of the DF test batches was monitored daily by measuring the gas pressure
8 in the headspace. The biogas composition (CO₂, O₂, H₂, N₂ and CH₄) was measured using a
9 gas chromatograph (Clarus 580, Perkin Elmer) coupled to a thermal conductivity detector
10 (TCD) [28].

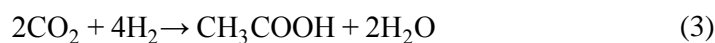
11 Ammonium (NH₄⁺) and phosphate (PO₄³⁻) ions were quantified using an ion chromatography
12 system (ICS 3000 Dionex, USA), as described elsewhere [29].

13 **3 Results and discussion**

14 **3.1 Dark fermentation test batches**

15 DF anaerobic test batches were carried out to provide a culture medium for subsequent
16 heterotrophic microalgae growth. The fermentation ended with complete glucose exhaustion,
17 after 6 days of fermentation. The final acetate and butyrate concentrations were 1.09 ± 0.09 g
18 L⁻¹ and 1.43 ± 0.07 g L⁻¹, respectively. No other fermentation metabolites, i.e. lactate, ethanol,
19 propionate, valerate and caproate, were found. The hydrogen yield, i.e. the molar ratio of
20 hydrogen produced per mol of glucose consumed, was 1.37 ± 0.18 mol H₂ mol glucose⁻¹. The
21 hydrogen yield was consistent with previously reported experimental results obtained in
22 similar conditions with mixed cultures [28]. The molar ratio of H₂ per mol of VFAs, the sum
23 of acetate and butyrate produced, was 1.1 ± 0.14 mol H₂ mol VFAs⁻¹. This value is lower than

1 the theoretical value of 2 mol H₂ mol VFAs⁻¹ produced through the acetate pathway (eq (1))
2 or the butyrate pathway (eq (2)). In general, the H₂ yield can be lowered either by the
3 consumption of glucose through non-hydrogen-producing pathways, such as ethanol or lactate
4 pathways, or by the direct consumption of H₂ through homoacetogenesis, i.e. the production
5 of acetate via CO₂ and H₂ consumption (eq (3)) [28]. Since neither lactate nor ethanol was
6 found, only homoacetogenesis could have occurred.



7 Three samples of DF effluent were sequenced for microbial community characterization. The
8 closest phylogenetically known sequences of the most representative OTUs are given in Table
9 1. About 53 ± 1.5 % of initial bacteria were strict anaerobes, with 36.8 ± 1.3% related to
10 *Clostridium* sp. and 16.2 ± 0.6% to *Sporolactobacillus* sp. It has been established that bacteria
11 belonging to *Clostridium* genus are responsible for hydrogen fermentation. *Sporolactobacillus*
12 sp. are known for their ability to degrade glucose to lactate in anaerobic conditions [30]. Since
13 no lactate was found in the medium and *Clostridium tyrobutyricum* was the most abundant
14 species, this suggested that lactate might have been converted into butyrate and hydrogen, as
15 previously reported [31]. *C. tyrobutyricum* is also known to use the butyrate pathway
16 preferentially during DF. The presence of this species would explain the high butyrate:acetate
17 molar ratio, 1.14, found at the end of DF [32].

18 The remaining bacteria were either facultative or strict aerobic species. Strict aerobes were
19 previously found in an anaerobic digester, even non-spore producing species [33]. Even
20 though the anaerobic sludge was heat treated before the fermentation, facultative and strict
21 aerobic bacteria may have survived, as reported elsewhere [30]. They in fact play an

1 important role in removing residual oxygen in anaerobic systems, which subsequently favors
2 the growth of *Clostridium* species and hydrogen production [34].

3 **3.2 Microalgae growth on raw fermentation effluent**

4 **3.2.1 Characterization of the dark fermentation effluent**

5 The initial acetate concentrations in the sterilized and unsterilized DF effluent samples were
6 $0.74 \pm 0.02 \text{ g L}^{-1}$ and $0.73 \pm 0.02 \text{ g L}^{-1}$, respectively. The initial butyrate concentrations in the
7 sterilized and unsterilized DF effluent samples were $1.25 \pm 0.06 \text{ g L}^{-1}$ and $1.26 \pm 0.03 \text{ g L}^{-1}$,
8 respectively. The acetate:butyrate mass ratio (g g^{-1}) was about 0.6 in both cases. These
9 concentrations as well as the acetate:butyrate ratio were consistent with previous studies using
10 raw DF effluents to sustain microalgae growth [11,35,36]. Sterilization by microfiltration had
11 no effect on the carbon, nitrogen and phosphorus contents of the effluent. The C:N:P molar
12 ratios in the sterilized and unsterilized DF effluent were 35:6.7:1 and 36:6.5:1, respectively.
13 These ratios were lower than the Redfield C:N:P ratio for phytoplankton cellular composition,
14 i.e. 106:16:1. Here, only the carbon substrate was assumed to be the limiting element for *C.*
15 *sorokiniana* growth.

16 Interestingly, other authors used effluents from acidogenic fermentation, instead of effluents
17 from DF, which contained high amounts of VFAs ranging from 5 to 14 g L^{-1} , to sustain
18 microalgae growth [12,37]. In acidogenic fermentation, VFA accumulation is targeted rather
19 than biohydrogen production and hydrogen conversion to acetate through homoacetogenesis
20 is promoted. Nevertheless, the effluents from acidogenic fermentation have to be diluted
21 between 8 and 20 fold before use to avoid excess initial VFA concentrations inhibiting
22 microalgae growth [12,37].

1 **3.2.2 Microalgae growth on sterilized and unsterilized dark fermentation effluent**
2 *C. sorokiniana* was grown for 10 days on sterilized and unsterilized DF effluent in
3 heterotrophic conditions (Figures 1 and 2, respectively). Microalgae grew during the first 2.7
4 days in both experiments. There was very similar growth in microalgae, expressed as the
5 logarithm of the number of 18S rDNA copies per mL of culture sample reaching 8.13 ± 0.05
6 and $8.20 \pm 0.04 \log(18S \text{ copies mL}^{-1})$ during growth on sterilized and unsterilized DF
7 effluent, respectively (Figure 2). The maximum CDW during heterotrophic cultivation on
8 sterilized DF effluent reached $0.33 \pm 0.01 \text{ g L}^{-1}$. In both conditions, microalgae concentration
9 did not increase during the last 7 days. Acetate was completely exhausted after 2.7 days in
10 both experiments (Figures 1 and 2). Butyrate was not consumed when axenic *C. sorokiniana*
11 was grown on sterilized DF effluent (Figure 1). On the other hand, butyrate degradation
12 started after complete acetate exhaustion and ended after 8 to 9 days when *C. sorokiniana* was
13 grown on unsterilized DF effluent (Figure 2). We concluded that *C. sorokiniana* grew in both
14 experiments using acetate until it was completely exhausted and that the bacterial community
15 initially present in unsterilized DF effluent was responsible for butyrate degradation. Since
16 very similar microalgae biomass yields were reached during both experiments, *C. sorokiniana*
17 was probably responsible for the complete exhaustion of acetate, despite the presence of a DF
18 bacterial community. This suggested that *C. sorokiniana* successfully outcompeted DF
19 bacteria for acetate uptake. The abrupt shift from anaerobic to aerobic culture conditions
20 might have hampered DF bacterial growth and enabled microalgae to degrade acetate without
21 competition with bacteria. It was clear that microalgae heterotrophic growth was favored in a
22 medium supplemented by raw DF effluent.

23 The maximum growth rate, μ_{\max} , of the microalgae was assessed during the exponential
24 growth phase and was $1.75 \pm 0.14 \text{ d}^{-1}$ on sterilized DF effluent. This μ_{\max} value was consistent
25 with previously reported growth rates of *C. sorokiniana* on acetate under heterotrophic

1 conditions at 25 °C [10]. During growth on sterilized DF effluent, the biomass yield, i.e. the
2 carbon taken from the substrate and incorporated into the biomass, was $55 \pm 4\%$. A similar
3 carbon yield of 52% was also reported with a mixotrophic culture of *Chlorella vulgaris* on
4 raw acidogenic fermentation effluent [9]. Interestingly, this yield is significantly higher than
5 previous values reported on synthetic DF effluents, 42% and 44%, for *C. sorokiniana* and *C.*
6 *protothecoides*, respectively [3,10]. In raw DF effluents, compounds other than VFAs, such as
7 amino acids and proteins, are available for microalgae growth [8]. The uptake of such
8 compounds by microalgae for their own growth could explain the higher yield on acetate
9 found in this study.

10 **3.3 Bacterial growth and diversity during microalgae cultivation on raw** 11 **fermentation effluent**

12 Bacterial growth was monitored using quantitative PCR during the experiment on unsterilized
13 DF effluent (Figure 3). The bacterial primers were tested on axenic *C. sorokiniana* samples.
14 DNA amplification was observed, probably because the primers matched chloroplast rDNA
15 sequences. However, due to the high initial load of bacteria, the number of 16S rDNA copies
16 due to microalgae was insignificant compared with the copies due to bacteria (data not
17 shown). Therefore, the results presented in Figure 3 were considered to be the result of
18 bacterial growth. Bacterial growth had two phases. The first growth period occurred during
19 acetate exhaustion from the beginning of the experiment to 2.7 days, during the *C.*
20 *sorokiniana* growth phase (Fig. 2). The logarithm of the number of 16S rDNA copies per mL
21 of culture sample started at 9.06 ± 0.22 and ended at 10.04 ± 0.22 after 2.7 days. As it was
22 suggested that acetate degradation resulted mainly from microalgae activity, the bacterial
23 community probably used other organic compounds initially present in the raw DF effluent or
24 released by microalgae. The second bacterial growth period started with butyrate degradation,
25 and bacterial biomass reached $11.01 \pm 0.4 \log$ (16S rDNA copies mL^{-1}) on day 7. During

1 butyrate degradation, the butyrate concentration was probably too high to support microalgae
2 growth, as previously suggested [10,35]. No competition was observed between microalgae
3 and bacteria for butyrate. The bacterial community was responsible for the entire butyrate
4 degradation. Butyrate exhaustion by bacteria could be very useful for the efficient cultivation
5 of microalgae on DF effluent. To produce high densities of microalgae and/or lipids, fed-
6 batch cultivation has been suggested, i.e. sequential addition of medium after exhaustion of
7 the substrate or when the growth plateau is reached [38]. For biomass production, this
8 technique avoids growth inhibition due to high initial substrate concentration and substrate
9 concentration is maintained at less than the inhibitory concentration during the process [38].
10 This strategy has been successfully used to produce high concentrations of lipids, 40 g L⁻¹, by
11 heterotrophic cultivation of *C. sorokiniana* on glucose [39]. If such operational conditions
12 were applied using sterilized DF effluent, butyrate would accumulate as a result of the
13 inability of *C. sorokiniana* to consume butyrate rapidly and would eventually lead to growth
14 inhibition [10]. Therefore, butyrate degradation by bacteria may be beneficial for lipid
15 production by heterotrophic microalgae, suggesting that bacteria may have a positive effect, if
16 well managed, for upscaling using unsterilized DF effluent.

17 The bacterial community in the raw effluent was dominated by 13 OTUs each with a relative
18 abundance of more than 2% at the start of the experiment, at acetate exhaustion or at the end
19 of the experiment. As shown in Figure 4, there were significant shifts in the bacterial
20 community during the experiment. The dominant bacterial species shifted from strict
21 anaerobes (*Clostridium sp.* and *Sporolactobacillus sp.*) to facultative anaerobes (*Paenibacillus*
22 *sp.*) and then to strict aerobes (*Stenotrophomonas maltophilia*). The dominant bacteria at the
23 beginning of the experiment (over 73% of the total bacteria abundance) accounted for less
24 than 3.5% of the bacteria present at day 2.7 when a species close to *Paenibacillus chibensis*
25 was dominant (over 60% of total bacteria) in two of the replicates (Figure 4). In only one of

1 the three replicates (flask 3), a high abundance (42.5%) of a species close to *Lysinibacillus*
2 *xylanilyticus* was observed with a reduction in the abundance of a species close to
3 *Paenibacillus chibensis*, (36.2%). According to Swezey *et al.* [40], *Paenibacillus chibensis* is
4 unable to grow on acetate. The presence of a dominant species closely related to
5 *Paenibacillus chibensis* (99% identity) suggested that acetate exhaustion by this species was
6 unlikely. Because acetate degradation was very similar in all replicates when unsterilized DF
7 effluent was used (Figure 3), the emergence of a different species closely related to
8 *Lysinibacillus xylanilyticus* in only one of the replicates, suggested that this species was
9 probably not involved in the exhaustion of acetate. These two observations were consistent
10 with and reinforced our previous suggestion that *C. sorokiniana* was highly competitive and
11 mainly responsible for acetate exhaustion.

12 At the end of the experiment, after complete butyrate exhaustion in the three replicate flasks,
13 species close to *Stenotrophomonas maltophilia* and *Cupriavidus necator*, both strict aerobic
14 species, were largely dominant (Figure 4) [33]. *Cupriavidus necator* is known to assimilate
15 butyrate and then produce polyhydroxyalkanoates [41]. The emergence of these bacterial
16 species during this period, during which no growth of *C. sorokiniana* was observed,
17 confirmed that strict aerobic bacterial species initially present in the raw DF effluent were
18 responsible for the butyrate uptake.

19 The results of this study clearly showed that the two main obstacles to industrial microalgae
20 cultivation in heterotrophic conditions, i.e. glucose and medium sterilization costs, could be
21 easily overcome by using unsterilized DF effluent. Firstly, acetate uptake by *C. sorokiniana*
22 was fast and sufficiently efficient to enable microalgae to outcompete bacteria. Secondly, the
23 abrupt change in the operational parameters between DF and heterotrophic cultivation, i.e.
24 from anaerobic culture conditions at 37 °C to aerobic culture conditions at 25 °C, favored

1 microalgae growth and may be a solution to avoid sterilization. Further research to find means
2 of reducing butyrate inhibition would have considerable potential.

3 **4 Conclusions**

4 This study showed the feasibility of using unsterilized dark fermentation effluent for
5 heterotrophic cultivation of microalgae. Microalgae successfully outcompeted bacteria
6 originating from DF effluent for acetate and achieved a carbon yield of 55%. The butyrate
7 concentration was too high to support microalgae growth but can be degraded by the aerobic
8 bacterial species initially present in the raw DF effluent. The use of a fed-batch mode for
9 heterotrophic cultivation of microalgae using raw DF effluent is proposed with the medium
10 being added at periods set to allow DF bacteria to exhaust the butyrate to prevent
11 accumulation and thus allowing microalgae to grow on acetate and accumulate lipids.
12 However, further research is required to assess the potential competitive role of the strict
13 aerobic bacterial community usually found with non-axenic cultivated microalgae.

14 **5 References**

- 15 [1] S. Venkata Mohan, M.V. Rohit, P. Chiranjeevi, R. Chandra, B. Navaneeth,
16 Heterotrophic Microalgae Cultivation to Synergize Biodiesel Production with Waste
17 Remediation: Progress and Perspectives, *Bioresour. Technol.* in press (2014) 169–178.
18 doi:10.1016/j.biortech.2014.10.056.
- 19 [2] G. Markou, E. Nerantzis, Microalgae for high-value compounds and biofuels
20 production: a review with focus on cultivation under stress conditions., *Biotechnol.*
21 *Adv.* 31 (2013) 1532–42. doi:10.1016/j.biotechadv.2013.07.011.
- 22 [3] Q. Fei, R. Fu, L. Shang, C.J. Brigham, H.N. Chang, Lipid production by microalgae
23 *Chlorella protothecoides* with volatile fatty acids (VFAs) as carbon sources in
24 heterotrophic cultivation and its economic assessment., *Bioprocess Biosyst. Eng.*
25 (2014) 691–700. doi:10.1007/s00449-014-1308-0.
- 26 [4] G.W. Park, Q. Fei, K. Jung, H.N. Chang, Y.-C. Kim, N.-J. Kim, et al., Volatile fatty
27 acids derived from waste organics provide an economical carbon source for microbial

- 1 lipids/biodiesel production., *Biotechnol. J.* 9 (2014) 1536–46.
2 doi:10.1002/biot.201400266.
- 3 [5] C. Sambusiti, M. Bellucci, A. Zabaniotou, L. Beneduce, F. Monlau, Algae as
4 promising feedstocks for fermentative biohydrogen production according to a
5 biorefinery approach: A comprehensive review, *Renew. Sustain. Energy Rev.* 44
6 (2015) 20–36. doi:10.1016/j.rser.2014.12.013.
- 7 [6] W.S. Lee, A.S.M. Chua, H.K. Yeoh, G.C. Ngoh, A review of the production and
8 applications of waste-derived volatile fatty acids, *Chem. Eng. J.* 235 (2014) 83–99.
9 doi:10.1016/j.cej.2013.09.002.
- 10 [7] H.-Y. Ren, B.-F. Liu, F. Kong, L. Zhao, D. Xing, N.-Q. Ren, Enhanced energy
11 conversion efficiency from high strength synthetic organic wastewater by sequential
12 dark fermentative hydrogen production and algal lipid accumulation, *Bioresour.*
13 *Technol.* 157 (2014) 355–359. doi:10.1016/j.biortech.2014.02.009.
- 14 [8] R.R. Singhanian, A.K. Patel, G. Christophe, P. Fontanille, C. Larroche, Biological
15 upgrading of volatile fatty acids, key intermediates for the valorization of biowaste
16 through dark anaerobic fermentation., *Bioresour. Technol.* (2012).
17 doi:10.1016/j.biortech.2012.12.137.
- 18 [9] H.U. Cho, Y.M. Kim, Y.-N. Choi, X. Xu, D.Y. Shin, J.M. Park, Effects of pH control
19 and concentration on microbial oil production from *Chlorella vulgaris* cultivated in the
20 effluent of a low-cost organic waste fermentation system producing volatile fatty
21 acids., *Bioresour. Technol.* (2014). doi:10.1016/j.biortech.2014.09.069.
- 22 [10] V. Turon, C. Baroukh, E. Trably, E. Latrille, E. Fouilland, J.-P. Steyer, Use of
23 fermentative metabolites for heterotrophic microalgae growth: Yields and kinetics,
24 *Bioresour. Technol.* 175 (2015) 342–349. doi:10.1016/j.biortech.2014.10.114.
- 25 [11] C.-H. Liu, C.-Y. Chang, Q. Liao, X. Zhu, C.-F. Liao, J.-S. Chang, Biohydrogen
26 production by a novel integration of dark fermentation and mixotrophic microalgae
27 cultivation, *Int. J. Hydrogen Energy.* 38 (2013) 15807–15814.
28 doi:10.1016/j.ijhydene.2013.05.104.
- 29 [12] B. Hu, W. Zhou, M. Min, Z. Du, P. Chen, X. Ma, et al., Development of an effective
30 acidogenically digested swine manure-based algal system for improved wastewater
31 treatment and biofuel and feed production, *Appl. Energy.* 107 (2013) 255–263.
32 doi:10.1016/j.apenergy.2013.02.033.
- 33 [13] M. Moon, C.W. Kim, W.-K. Park, G. Yoo, Y.-E. Choi, J.-W. Yang, Mixotrophic
34 growth with acetate or volatile fatty acids maximizes growth and lipid production in
35 *Chlamydomonas reinhardtii*, *Algal Res.* 2 (2013) 352–357.
36 doi:10.1016/j.algal.2013.09.003.
- 37 [14] E.A. Ramos Tercero, E. Sforza, M. Morandini, A. Bertucco, Cultivation of *Chlorella*
38 *protothecoides* with urban wastewater in continuous photobioreactor: biomass
39 productivity and nutrient removal., *Appl. Biochem. Biotechnol.* 172 (2014) 1470–85.
40 doi:10.1007/s12010-013-0629-9.

- 1 [15] N. Rashid, M.S. Ur Rehman, M. Sadiq, T. Mahmood, J.-I. Han, Current status, issues
2 and developments in microalgae derived biodiesel production, *Renew. Sustain. Energy*
3 *Rev.* 40 (2014) 760–778. doi:10.1016/j.rser.2014.07.104.
- 4 [16] Y. Zhang, H. Su, Y. Zhong, C. Zhang, Z. Shen, W. Sang, et al., The effect of bacterial
5 contamination on the heterotrophic cultivation of *Chlorella pyrenoidosa* in wastewater
6 from the production of soybean products., *Water Res.* 46 (2012) 5509–16.
7 doi:10.1016/j.watres.2012.07.025.
- 8 [17] N. Kamjunke, B. Köhler, N. Wannicke, J. Tittel, Algae As Competitors for Glucose
9 With Heterotrophic Bacteria, *J. Phycol.* 44 (2008) 616–623. doi:10.1111/j.1529-
10 8817.2008.00520.x.
- 11 [18] L. Ramanna, A. Guldhe, I. Rawat, F. Bux, The optimization of biomass and lipid yields
12 of *Chlorella sorokiniana* when using wastewater supplemented with different nitrogen
13 sources., *Bioresour. Technol.* 168 (2014) 127–35. doi:10.1016/j.biortech.2014.03.064.
- 14 [19] M. Pierra, E. Trably, J.-J. Godon, N. Bernet, Fermentative hydrogen production under
15 moderate halophilic conditions, *Int. J. Hydrogen Energy.* (2013) 1–10.
16 doi:10.1016/j.ijhydene.2013.08.035.
- 17 [20] F. Chen, M.R. Johns, Relationship between substrate inhibition and maintenance
18 energy of *Chlamydomonas reinhardtii* in heterotrophic culture, *J. Appl. Phycol.* 8
19 (1996) 15–19.
- 20 [21] J.N. Rosenberg, N. Kobayashi, A. Barnes, E.A. Noel, M.J. Betenbaugh, G.A. Oyler,
21 Comparative analyses of three *Chlorella* species in response to light and sugar reveal
22 distinctive lipid accumulation patterns in the Microalga *C. sorokiniana*., *PLoS One.* 9
23 (2014) e92460. doi:10.1371/journal.pone.0092460.
- 24 [22] R. Hoshina, Y. Kato, S. Kamako, N. Imamura, Genetic evidence of “American” and
25 “European” type symbiotic algae of *Paramecium bursaria* Ehrenberg., *Plant Biol.*
26 (Stuttg). 7 (2005) 526–32. doi:10.1055/s-2005-865912.
- 27 [23] Y. Yu, C. Lee, J. Kim, S. Hwang, Group-specific primer and probe sets to detect
28 methanogenic communities using quantitative real-time polymerase chain reaction.,
29 *Biotechnol. Bioeng.* 89 (2005) 670–9. doi:10.1002/bit.20347.
- 30 [24] A. Abbassi-Guendouz, E. Trably, J. Hamelin, C. Dumas, J.P. Steyer, J.-P. Delgenès, et
31 al., Microbial community signature of high-solid content methanogenic ecosystems.,
32 *Bioresour. Technol.* 133 (2013) 256–62. doi:10.1016/j.biortech.2013.01.121.
- 33 [25] J.J. Kozich, S.L. Westcott, N.T. Baxter, S.K. Highlander, P.D. Schloss, Development
34 of a dual-index sequencing strategy and curation pipeline for analyzing amplicon
35 sequence data on the MiSeq Illumina sequencing platform., *Appl. Environ. Microbiol.*
36 79 (2013) 5112–20. doi:10.1128/AEM.01043-13.
- 37 [26] P.D. Schloss, S.L. Westcott, T. Ryabin, J.R. Hall, M. Hartmann, E.B. Hollister, et al.,
38 Introducing mothur: open-source, platform-independent, community-supported

- 1 software for describing and comparing microbial communities., *Appl. Environ.*
2 *Microbiol.* 75 (2009) 7537–41. doi:10.1128/AEM.01541-09.
- 3 [27] S.F. Altschul, W. Gish, W. Miller, E.W. Myers, D.J. Lipman, Basic Local Alignment
4 Search Tool, (1990).
- 5 [28] Y. Rafrafi, E. Trably, J. Hamelin, E. Latrille, I. Meynial-Salles, S. Benomar, et al.,
6 Sub-dominant bacteria as keystone species in microbial communities producing bio-
7 hydrogen, *Int. J. Hydrogen Energy.* 38 (2013) 4975–4985.
8 doi:10.1016/j.ijhydene.2013.02.008.
- 9 [29] E. Uggetti, B. Sialve, E. Latrille, J.-P. Steyer, Anaerobic digestate as substrate for
10 microalgae culture: the role of ammonium concentration on the microalgae
11 productivity., *Bioresour. Technol.* 152 (2014) 437–43.
12 doi:10.1016/j.biortech.2013.11.036.
- 13 [30] N.M.C. Saady, Homoacetogenesis during hydrogen production by mixed cultures dark
14 fermentation: Unresolved challenge, *Int. J. Hydrogen Energy.* 38 (2013) 13172–13191.
15 doi:10.1016/j.ijhydene.2013.07.122.
- 16 [31] C.-W. Wu, L.-M. Whang, H.-H. Cheng, K.-C. Chan, Fermentative biohydrogen
17 production from lactate and acetate., *Bioresour. Technol.* 113 (2012) 30–6.
18 doi:10.1016/j.biortech.2011.12.130.
- 19 [32] Y. Zhu, S.-T. Yang, Effect of pH on metabolic pathway shift in fermentation of xylose
20 by *Clostridium tyrobutyricum.*, *J. Biotechnol.* 110 (2004) 143–57.
21 doi:10.1016/j.jbiotec.2004.02.006.
- 22 [33] E.A. Assih, A.S. Ouattara, S. Thierry, J.L. Cayol, M. Labat, H. Macarie,
23 *Stenotrophomonas acidaminiphila* sp. nov., a strictly aerobic bacterium isolated from
24 an upflow anaerobic sludge blanket (UASB) reactor, *Int. J. Syst. Evol. Microbiol.* 52
25 (2002) 559–568.
- 26 [34] C.-H. Hung, Y.-T. Chang, Y.-J. Chang, Roles of microorganisms other than
27 *Clostridium* and *Enterobacter* in anaerobic fermentative biohydrogen production
28 systems - A review, *Bioresour. Technol.* 102 (2011) 8437–44.
29 doi:10.1016/j.biortech.2011.02.084.
- 30 [35] C.-H. Liu, C.-Y. Chang, Q. Liao, X. Zhu, J.-S. Chang, Photoheterotrophic growth of
31 *Chlorella vulgaris* ESP6 on organic acids from dark hydrogen fermentation effluents.,
32 *Bioresour. Technol.* 145 (2012) 331–336. doi:10.1016/j.biortech.2012.12.111.
- 33 [36] S. Venkata Mohan, M. Prathima Devi, Fatty acid rich effluent from acidogenic
34 biohydrogen reactor as substrate for lipid accumulation in heterotrophic microalgae
35 with simultaneous treatment., *Bioresour. Technol.* 123 (2012) 627–35.
36 doi:10.1016/j.biortech.2012.07.004.
- 37 [37] B. Hu, M. Min, W. Zhou, Z. Du, M. Mohr, P. Chen, et al., Enhanced mixotrophic
38 growth of microalga *Chlorella* sp. on pretreated swine manure for simultaneous biofuel

- 1 feedstock production and nutrient removal., *Bioresour. Technol.* 126C (2012) 71–79.
2 doi:10.1016/j.biortech.2012.09.031.
- 3 [38] F. Bumbak, S. Cook, V. Zachleder, S. Hauser, K. Kovar, Best practices in
4 heterotrophic high-cell-density microalgal processes: achievements, potential and
5 possible limitations., *Appl. Microbiol. Biotechnol.* 91 (2011) 31–46.
6 doi:10.1007/s00253-011-3311-6.
- 7 [39] Y. Zheng, T. Li, X. Yu, P.D. Bates, T. Dong, S. Chen, High-density fed-batch culture
8 of a thermotolerant microalga *Chlorella sorokiniana* for biofuel production, *Appl.*
9 *Energy*. 108 (2013) 281–287. doi:10.1016/j.apenergy.2013.02.059.
- 10 [40] J. Swezey, Emended Description of *Paenibacillus amylolyticus* and Description of
11 *Paenibacillus illinoisensis* sp . nov . and *Paenibacillus chibensis* sp . nov ., (1997) 299–
12 306.
- 13 [41] E. Grousseau, E. Blanchet, S. Déléris, M.G.E. Albuquerque, E. Paul, J.-L. Uribe Larrea,
14 Impact of sustaining a controlled residual growth on polyhydroxybutyrate yield and
15 production kinetics in *Cupriavidus necator*., *Bioresour. Technol.* 148 (2013) 30–8.
16 doi:10.1016/j.biortech.2013.08.120.
- 17 [42] N. a Logan, E. De Clerck, L. Lebbe, A. Verhelst, J. Goris, G. Forsyth, et al.,
18 *Paenibacillus cineris* sp. nov. and *Paenibacillus cookii* sp. nov., from Antarctic volcanic
19 soils and a gelatin-processing plant., *Int. J. Syst. Evol. Microbiol.* 54 (2004) 1071–6.
20 doi:10.1099/ijs.0.02967-0.
- 21 [43] I. Suominen, C. Spröer, P. Kämpfer, F.A. Rainey, K. Lounatmaa, M. Salkinoja-
22 Salonen, *Paenibacillus stellifer* sp. nov., a cyclodextrin-producing species isolated from
23 paperboard, *Int. J. Syst. Evol. Microbiol.* 53 (2003) 1369–1374.
24 doi:10.1099/ijs.0.02277-0.
- 25 [44] P. Vandamme, E.R.B. Moore, M. Cnockaert, C. Peeters, L. Svensson-Stadler, K. Houf,
26 et al., Classification of *Achromobacter* genogroups 2, 5, 7 and 14 as *Achromobacter*
27 *insuavis* sp. nov., *Achromobacter aegrifaciens* sp. nov., *Achromobacter anxifer* sp. nov.
28 and *Achromobacter dolens* sp. nov., respectively., *Syst. Appl. Microbiol.* 36 (2013)
29 474–82. doi:10.1016/j.syapm.2013.06.005.
- 30 [45] N. Boutros, N. Gonullu, *Ralstonia pickettii* traced in blood culture bottles, *J. Clin.*
31 40 (2002) 2666–2667. doi:10.1128/JCM.40.7.2666.
- 32 [46] B. Schiel-Bengelsdorf, P. Dürre, Pathway engineering and synthetic biology using
33 acetogens., *FEBS Lett.* 586 (2012) 2191–8. doi:10.1016/j.febslet.2012.04.043.

34

1

2 **6 Figure captions**

3 **Figure 1. Heterotrophic growth of *Chlorella sorokiniana* on sterilized dark fermentation** 4 **effluent**

5 Biomass growth in g L^{-1} (●), acetate concentration in g L^{-1} (■) and butyrate concentration in g
6 L^{-1} (◆) during heterotrophic growth on sterilized effluent

7 **Figure 2. Heterotrophic growth of *Chlorella sorokiniana* on unsterilized dark** 8 **fermentation effluent**

9 Logarithm of the number of target copies per mL of culture, using chlorophyta specific
10 primers for 18S rDNA, during heterotrophic growth on sterilized (●) and unsterilized (●)
11 effluent with the acetate concentration in g L^{-1} (■) and butyrate concentration in g L^{-1} (◆)
12 during heterotrophic growth on unsterilized effluent.

13 **Figure 3. Bacterial growth on unsterilized dark fermentation effluent**

14 Logarithm of the number of target copies per mL of culture, using bacterial primers for 16S
15 rDNA, during growth unsterile (●) effluent with acetate concentration in g L^{-1} (■) and
16 butyrate concentration in g L^{-1} (◆).

17 **Figure 4. Bacterial community diversity during aerobic growth on unsterilized dark** 18 **fermentation effluent**

19 Taxa with less than 2% of individual relative abundance were grouped under “Others”.

20

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This study was funded by the National Institute of Agronomic Research (INRA) and the University of Montpellier II, France.

Table 1.

Classification, relative abundance (%) and physiological characteristics of bacteria at the end of dark fermentation test batches.

ORDER /species (closest known sequence)¹	Relative abundance (%)²	Anaerobic or aerobic metabolism	Specific characteristics	Reference
BACILLALES				
<i>Paenibacillus chibensis</i>	3.17 ± 0.1	Strict aerobe	Spore producer Unable to grow on acetate	[40]
<i>Paenibacillus cookii</i>	8.21 ± 0.73	Facultative anaerobe	Spore producer	[42]
<i>Paenibacillus stellifer</i>	10.66 ± 0.91	Facultative anaerobe	Spore producer Unable to grow on acetate	[43]
<i>Sporolactobacillus laevus</i>	16.18 ± 0.65	Strict anaerobe	Spore producer, lactate producer	[30]
BURKHOLDERIALES				
<i>Achromobacter aegrifaciens</i>	3.12 ± 0.32	Strict aerobe	Acetate and butyrate consumer	[44]
<i>Ralstonia pickettii</i>	9.6 ± 0.36	Facultative anaerobe / Strict aerobe	Can grow under anaerobic conditions	[45]
CLOSTRIDIALES				
<i>Clostridium magnum</i>	8.12 ± 0.65	Strict anaerobe	Spore producer, homoacetogene	[46]
<i>Clostridium tyrobutyricum</i>	28.7 ± 0.66	Strict anaerobe	Spore producer, hydrogen producer	[31]
OTHERS³	12.23 ± 1.65			

¹: Names in bold letters correspond to the bacterial orders identified. Names in italics correspond to the closest genetically known sequences, for all sequences, percentages of identity to reference sequence were greater or equal to 97%.

²: Relative abundances were calculated by dividing the number of sequences for the taxon by the total number of sequences per sample. The values are the mean and standard deviation of the sequences from the three samples.

³: **Taxa** with less than 2% relative abundance were grouped under "Others".

Figure 1 (single column fitting image)

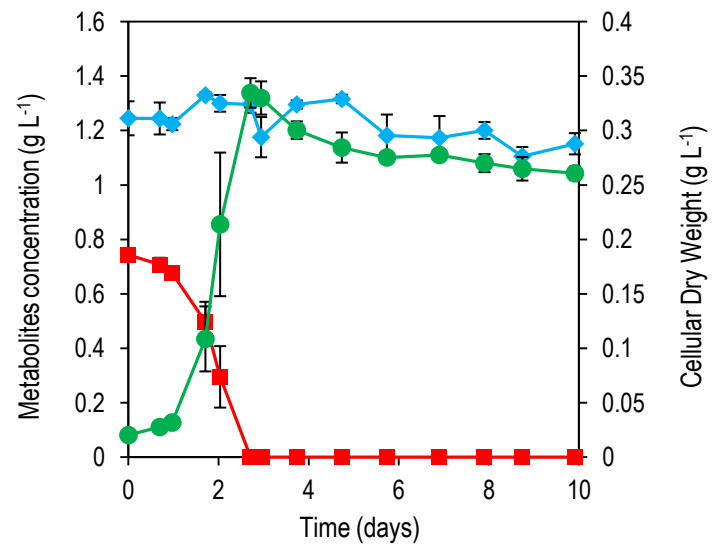


Figure 2 (single column fitting image)

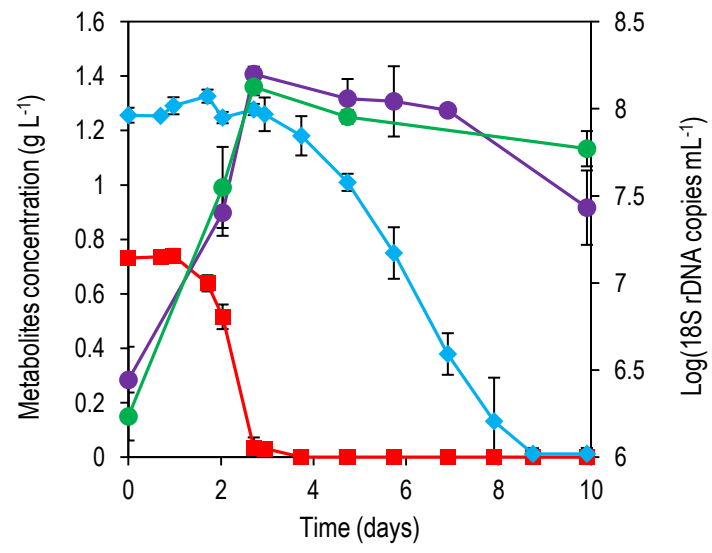


Figure 3 (single column fitting image)

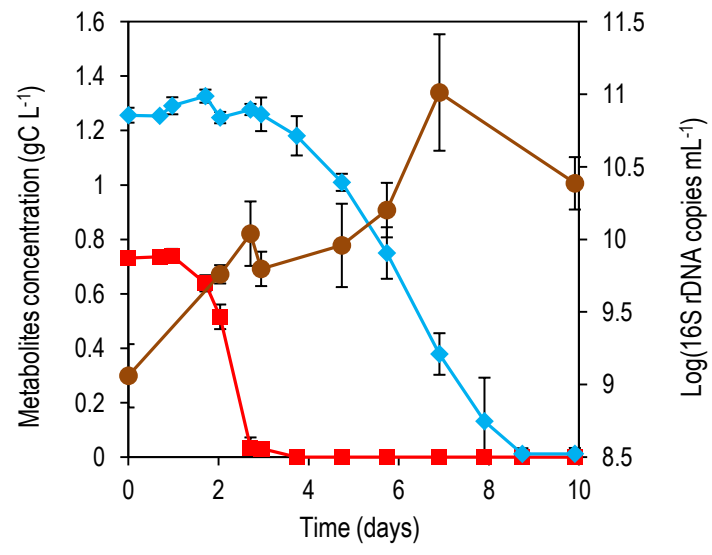


Figure 4 (2-column fitting image)

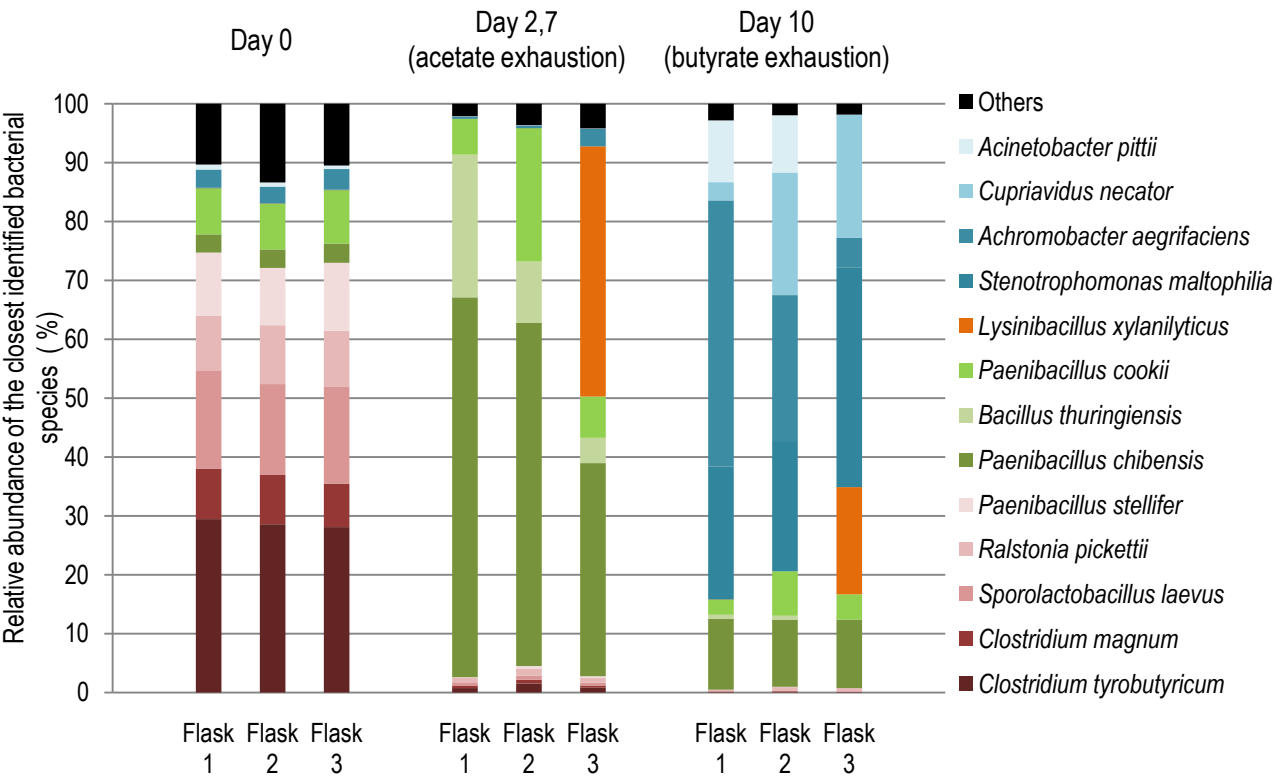


Figure 1 (single column fitting image)

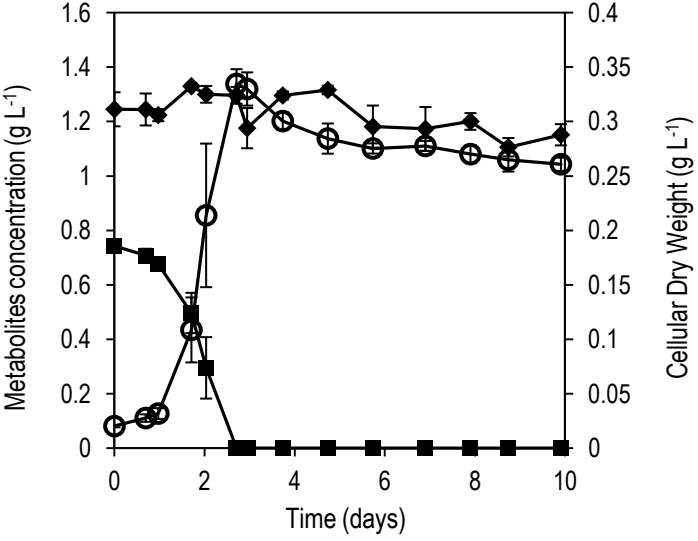


Figure 2 (single column fitting image)

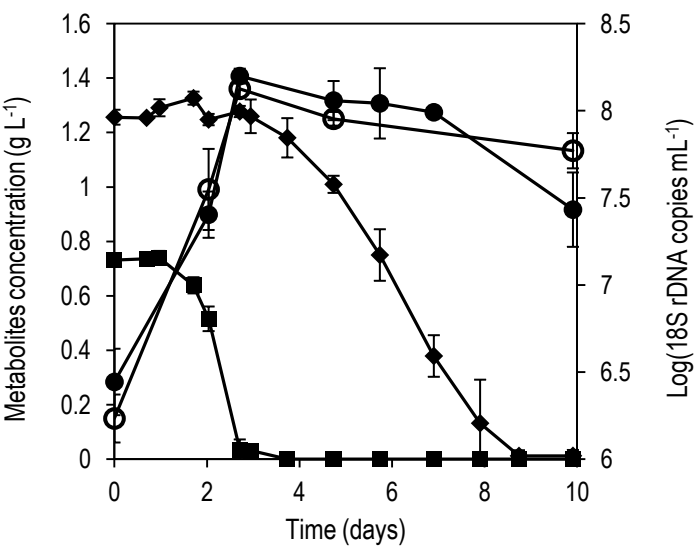
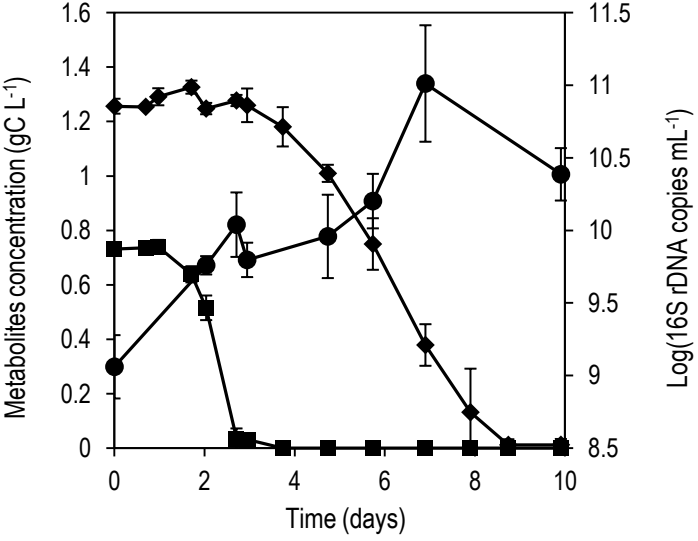
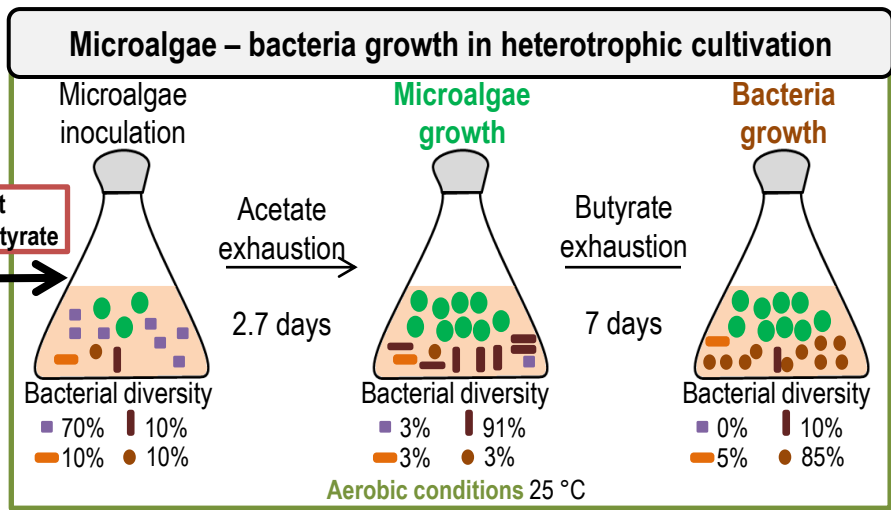
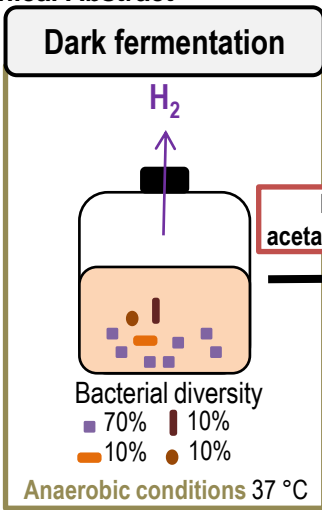


Figure 3 (single column fitting image)





Highlights

- Microalgae can outcompete dark fermentation bacteria for acetate uptake.
- Butyrate is not used by *Chlorella sorokiniana* in heterotrophic conditions.
- Bacteria originating from dark fermentation effluent can degrade butyrate.